

- Asymptotic limit at high p is $\theta=1$, as reflected in assumptions.
- Interaction between solid and gas is represented by the constant B . θ rises with B at a given pressure.

$$B = \frac{1}{kT} \left(\frac{q^{ads}}{\left(\frac{q^{gas}}{V} \right)} \right) \exp \left(\frac{\epsilon_o^{gas} - \epsilon_o^{ads}}{kT} \right)$$

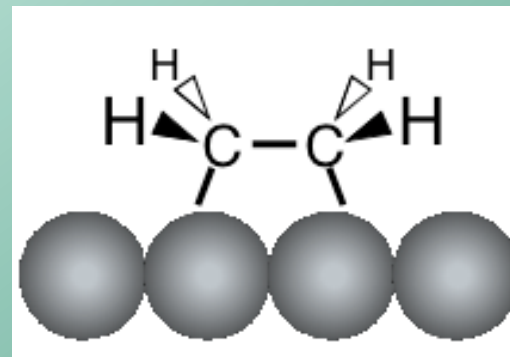
- Variation dominated by exponential i.e.
- $\epsilon^{gas} - \epsilon^{ads}$, the strength of the bond to the surface.
- T . B (and coverage) falls as T rises (exothermic process).

Typical numbers

- $q^{gas}/V = 2 \times 10^{32}$ for 40 amu atom, 300K
- $q^{ads} = 1$ (rigid surface bond)
- $\epsilon^{gas} - \epsilon^{ads} = 50 \text{ kJmol}^{-1}$ (typical surface bond)
- yields $\theta = 0.5$ at $P \sim 2000 \text{ Pa} \sim 10^{-2} \text{ atm.}$
- *i.e.* adsorption very readily occurs!

Is the Langmuir isotherm successful?

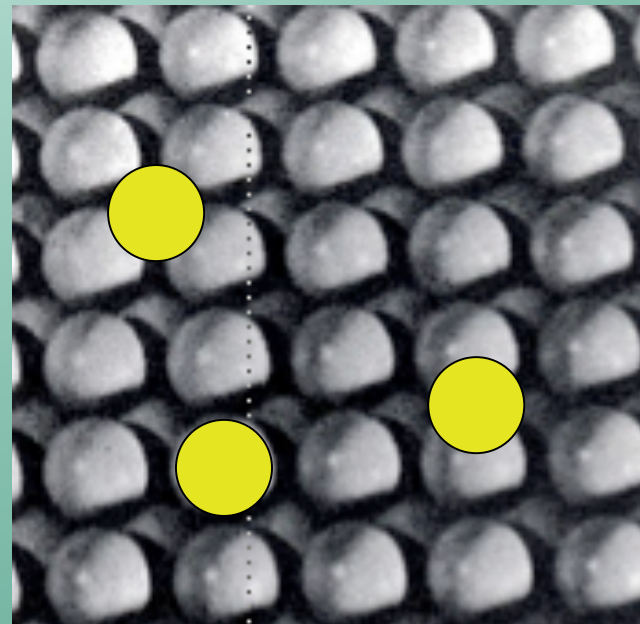
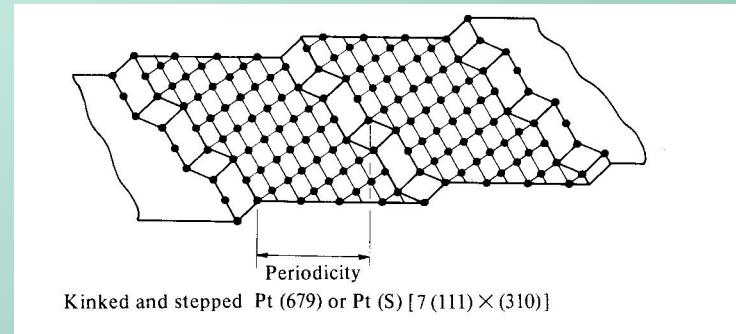
- Correct, at least qualitatively, for adsorption systems where the molecule chemically bonds to the surface.
“chemisorption”
- In these systems, adsorption beyond a monolayer is impossible.

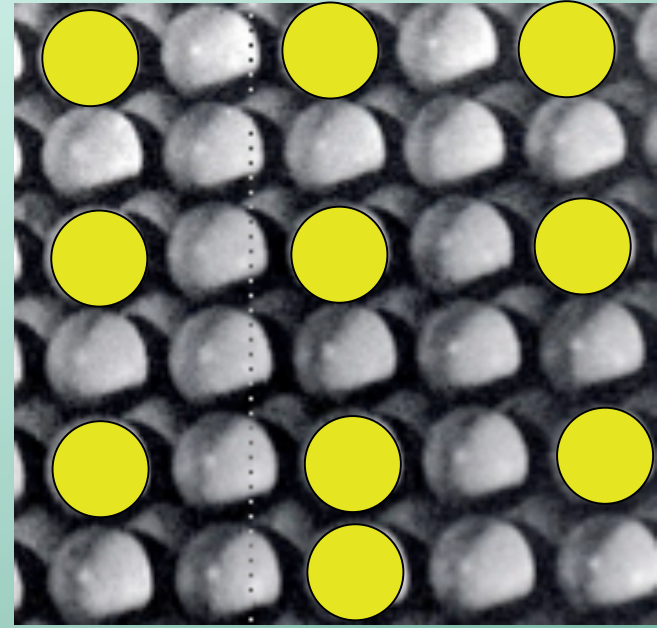
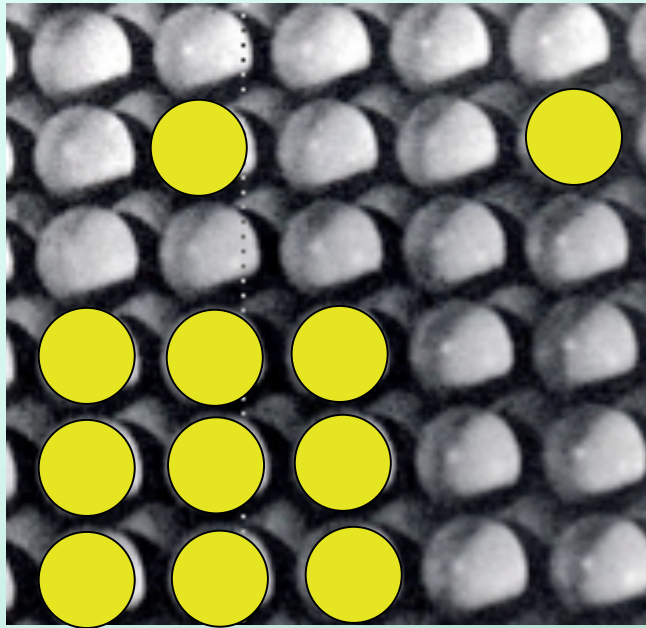


Quantitative failures in describing chemisorption systems

- Surfaces aren't uniform
- So the heat of adsorption isn't constant.

Even a structurally uniform surface can have different sites





- Adsorbed species can attract or repel each other.
- So adsorption can be ordered rather than random and again this causes variation in heat of adsorption

Any improvements?

- Various isotherms exist based on the “Langmuir” model but with heats of adsorption which vary with coverage in particular ways.
- Improve empirical representation of data, but yield little further insights into the surface chemistry involved.

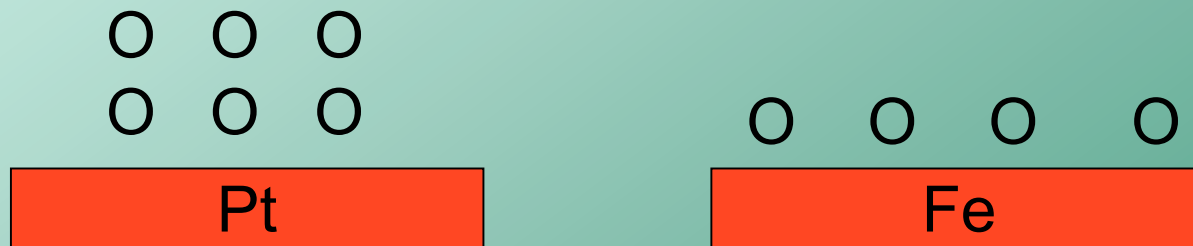
$$N^{ads} = \beta p^{1/\kappa} \quad \theta = \beta \ln(\kappa p)$$

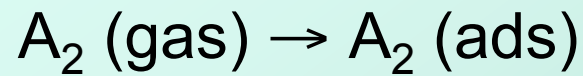
Freundlich

Temkin

Dissociative adsorption using Langmuir's approach

- On many surfaces, molecules tend to dissociate spontaneously
- Need to modify the equations

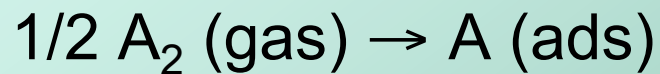




$$\mu^{gas} = \mu^{ads}$$

$$X - kT \ln \frac{1}{p} = Y - kT \ln \left(\frac{1}{\theta} - 1 \right)$$

$$\frac{1}{Bp} = \frac{1}{\theta} - 1$$



$$\frac{1}{2} \mu^{gas} = \mu^{ads}$$

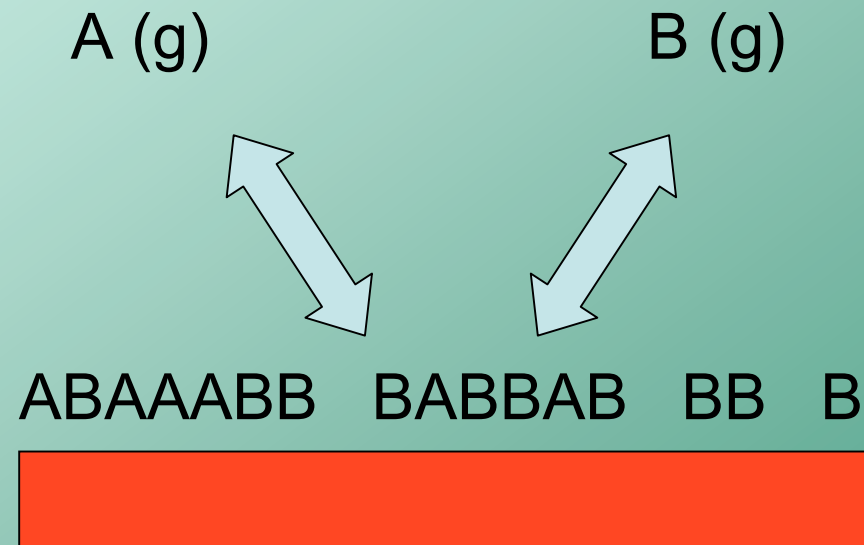
$$\frac{1}{2} \left(X - kT \ln \frac{1}{p} \right) = Y - kT \ln \left(\frac{1}{\theta} - 1 \right)$$

$$\frac{1}{Bp^{1/2}} = \frac{1}{\theta} - 1$$

$$\theta = \frac{Bp^{1/2}}{1 + Bp^{1/2}}$$

Competitive adsorption

- Can have 2 or more gas phase species adsorbing on the same surface
- If one species is adsorbed, the other is blocked - “competitive adsorption”



rate of ads. = rate of des.

$$k_A^{ads} (1 - \theta_A - \theta_B) p_A = k_A^{des} \theta_A$$

$$k_B^{ads} (1 - \theta_A - \theta_B) p_B = k_B^{des} \theta_B$$

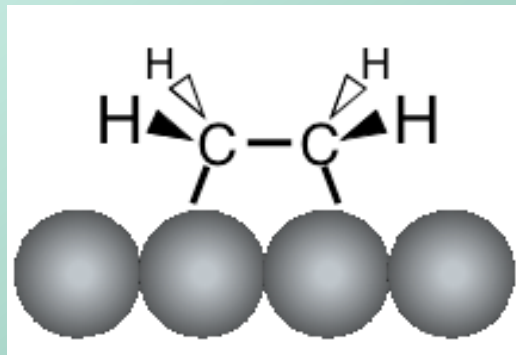
- Solve simultaneously for θ_A , θ_B

$$\theta_A = \frac{B_A P_A}{1 + B_A P_A + B_B P_B} \quad \theta_B = \frac{B_B P_B}{1 + B_A P_A + B_B P_B}$$

$$\theta_A = \frac{B_A P_A}{1 + \sum_i B_i P_i}$$

Physisorption

- Models and discussion above is relevant to chemisorption - chemical bond between adsorbate and surface.



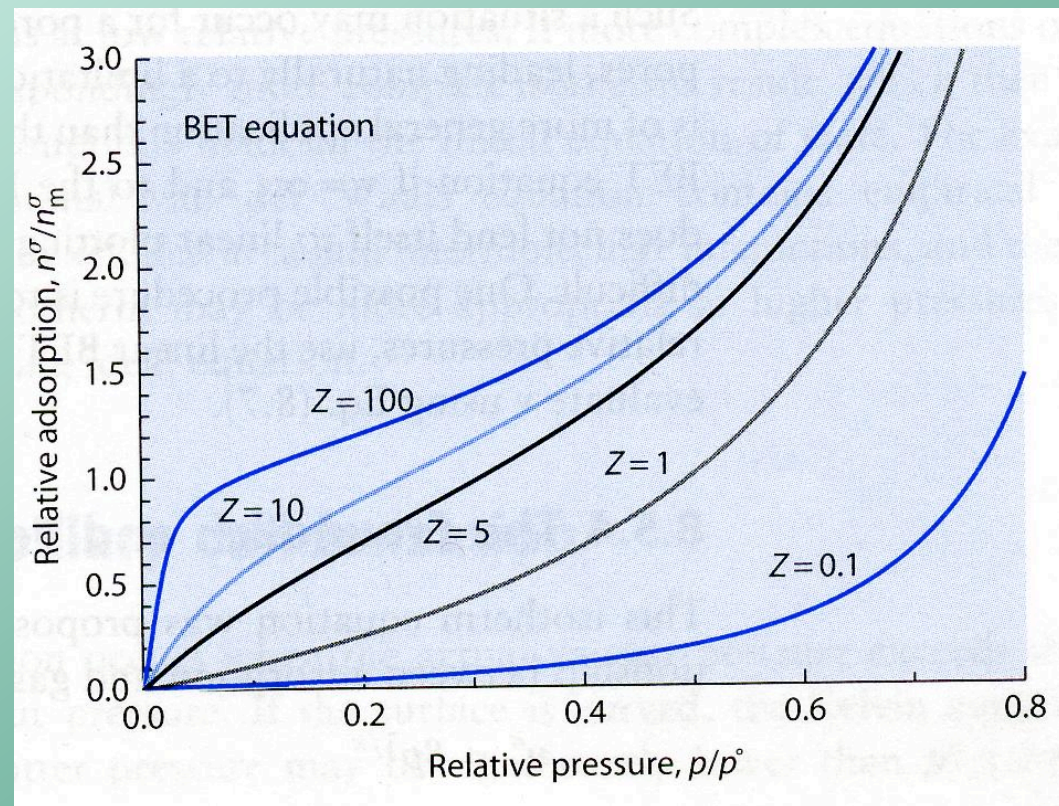
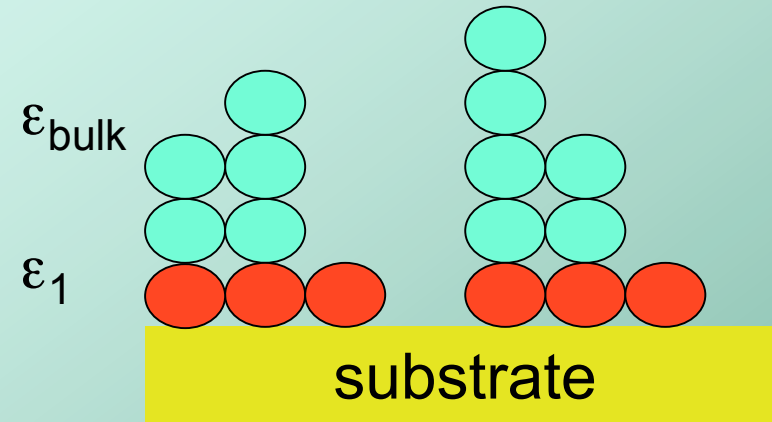
- But a second mode of adsorption exists “**physisorption**”
- Weak physical forces of interaction (dispersion, dipole etc.)
- ΔH_{ads} small ($< 20 \text{ kJ mol}^{-1}$)
- Related to condensation

Some characteristics of physisorption

- Observed universally (e.g. inert gases) in contrast to chemisorption.
- But significant pressures required because of low ΔH_{ads} .
- Best described in terms of the *relative pressure* p/p_0 where p_0 is the saturated vapour pressure.
- At high relative pressures (p/p_0 close to 1) observe multilayer formation.

- Molecule in first layer (mainly molecule-substrate forces)
- Molecule in multilayer phase (mainly molecule-molecule forces)

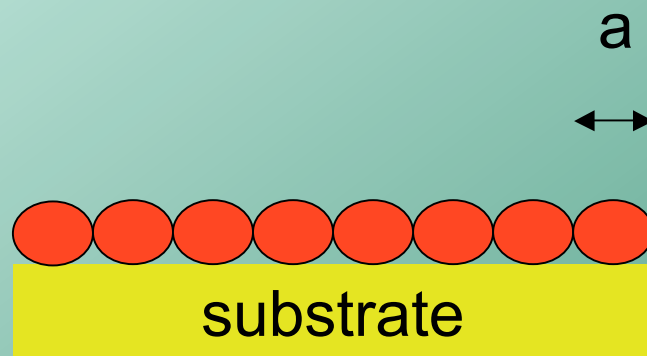
$$Z \approx \exp(\epsilon^{bulk} - \epsilon^1 / kT)$$



Some applications of the Langmuir isotherm

1. Measurement of the surface area of powders
e.g. pigments; absorbents (molecular sieves etc); phosphors; heterogeneous catalysts
 - Often have internal and external “surfaces”

- how many molecules (N^{ads}) are adsorbed when the surface is saturated with a molecule of cross-section “a”?
- Surface area = $N^{\text{ads}} \times a$
- So we need a reliable way of determining the “monolayer capacity”



- Re-write θ as x/x^m where
 - x is mass of gas adsorbed
 - x^m is mass of gas adsorbed at saturation (the unknown, same units as x)

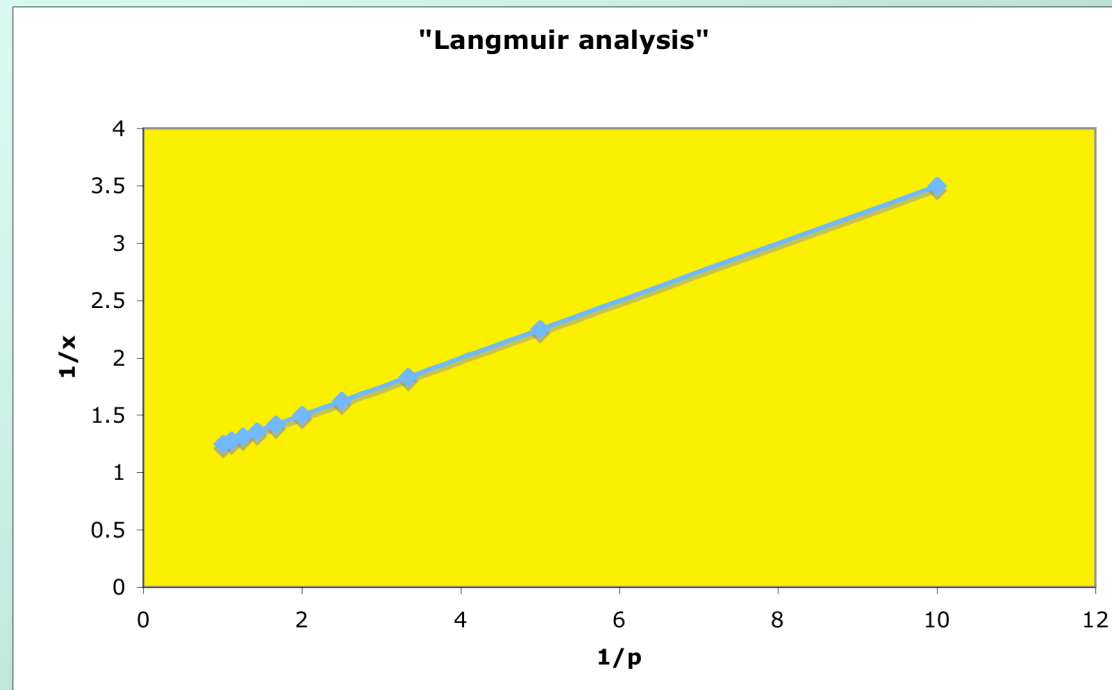
- So θ_A becomes

$$\theta_A = \frac{Bp_A}{1 + Bp_A} \quad \frac{x}{x^m} = \frac{Bp}{1 + Bp}$$

which rearranges to

$$\frac{1}{x} = \frac{1}{x^m Bp} + \frac{1}{x^m}$$

so measure x for differing p and plot $1/x$ vs $1/p$



According to above analysis, intercept = $1/x^m$
and Slope = $1/(x^m B)$ enabling both x^m and B
to be determined.

- If a = area of adsorbed molecule
 M = molecular weight (same units as x)
 S = surface area (same units as a)

$$S = \left(x^m / M \right) \times \left(N_{avo} \right) \times \left(a \right)$$

Note: this Langmuirian approach works best for *chemisorption* - area is the “reactive” surface. “Total” area can be determined using *physisorption* and an applicable isotherm (BET eq.)